

## **AMENDMENTS TO THE SPECIFICATION**

**Please delete the last full paragraph on page 6 bridging page 7 in the specification, and replace with the following new one:**

Fig. 1 shows an SEM (scanning electron microscope) image of metallic tellurium particles as obtained in Example 1.

Fig. 2 shows an SEM (scanning electron microscope) image of metallic tellurium particles as obtained in Example 2.

Fig. 3 shows an SEM (scanning electron microscope) image of metallic tellurium particles as obtained in Example 3.

**Please delete the second full paragraph on page 8 in the specification, and replace with the following new one:**

As reductants, any reducing substances (atoms, molecules or ions to be capable of providing other molecule with electrons)~~having properties so as to likely provide other molecule with electrons~~ having an oxidation-reduction potential against a standard electrode of not higher than 0.53 V (the potential of tellurium dioxide is in the vicinity of 0.53 V) can be used.

**Please delete the first full paragraph on page 9 in the specification, and replace with the following new one:**

For example, when hydrazine is used, the molar ratio of hydrazine to tellurium is preferably from 0.5 to 4.0, and more preferably from 1.0 to 3.0. When the amount of hydrazine added is less than 0.5 mole, unreacted tellurium dioxide remains in a large amount. On the other hand, when the amount of hydrazine added exceeds 4.0 moles, or more, even by further increasing the addition amount, there is no advantage at all. Rather, in order to remove

unreacted hydrazine, excessive labors and rinsing liquids are required. In the case of other reductants than hydrazine, the amount of their addition substantially follows that of hydrazine.

**Please delete the first full paragraph on page 12 in the specification, and replace with the following new one:**

When the foregoing dried powder of metallic tellurium is observed by an electron microscope, with respect to the appearance of the primary particle, a spherical particle or an acicular particle is observed depending upon the difference of the reduction method. Any primary particle has a very narrow particle size distribution. Furthermore, though agglomeration of the primary particle is seen depending upon the sample to be observed, this can be generated at the time of drying~~this is a phenomenon as generated at the time of drying the sample~~ and does not affect the production of a catalyst and the performance of the resulting catalyst.

**Please delete the second full paragraph on page 12 bridging page 13 in the specification, and replace with the following new one:**

The size of the primary particle of metallic tellurium as obtained by the foregoing reduction reaction is in the range of not more than 4.0  $\mu\text{m}$ , and preferably not more than 2.0  $\mu\text{m}$  in at least one direction. Though a lower limit of the size of the primary particle is not particularly present, it is preferably 0.01  $\mu\text{m}$  or more from the viewpoint of easiness of the operation. When the size of the primary particle is more than 4.0  $\mu\text{m}$ , ~~or more~~, dispersibility of the metallic tellurium particle in water or the organic solvent becomes worse so that the production of a catalyst is likely adversely affected thereby.

**Please delete the first full paragraph on page 14 in the specification, and replace with the following new one:**

In the step (3), the aqueous~~reducing~~ dispersion containing the metallic tellurium fine particle as obtained in the foregoing step (2) is mixed with an  $\text{Mo}^{6+}$  compound and a  $\text{V}^{5+}$  compound, and the mixture is allowed to react at a temperature of 40°C or higher for one hour or more.

**Please delete the third full paragraph on page 19 in the specification, and replace with the following new one:**

The space velocity (hereinafter referred to as "SV") of the whole of the raw material gases is suitably adjusted from 1,000 to 8,000  $\text{hr}^{-1}$ . When the space velocity is less than 1,000  $\text{hr}^{-1}$ , a yield of acrylic acid per unit mass of the catalyst becomes low, while when it exceeds 8,000  $\text{hr}^{-1}$ , the conversion is lowered.

**Please delete the first full paragraph on page 20 in the specification, and replace with the following new one:**

The metal oxide catalyst as obtained in each of the Examples was once tablet-molded, and the molded particle~~article~~ was pulverized into a size of from 16 to 30 mesh and provided for use.

**Please delete the second full paragraph on page 20 in the specification, and replace with the following new one:**

1.1 mL (about 1.0 g) of the catalyst as produced in each of the Examples was charged in a quartz-made reaction tube having an inner diameter of 10 mm. The reaction tube was heated at 400°C, and a mixed gas containing 6.4 % by volume of propane, 9.6 % by volume of oxygen, 36.1 % by volume of nitrogen and 47.7 % by volume of steam was fed into the reaction tube at a space velocity of 3,924  $\text{hr}^{-1}$ , thereby producing acrylic acid.

**Please delete the second full paragraph on page 22 in the specification, and replace with the following new one:**

As a result of the X-ray diffraction analysis, the resulting black powder exhibited diffraction lines at angles of 22.98, 27.52, 38.24, 40.42, 43.32, 45.88 and 49.62° in terms of  $2\theta$ , and the phase of tellurium dioxide was not detected. Thus, the black powder is assigned to a crystal line of pure metallic tellurium.~~a crystal phase of tellurium dioxide was not acknowledged~~. Thus, ~~it was noted that the black powder is a crystal of pure metallic tellurium~~.